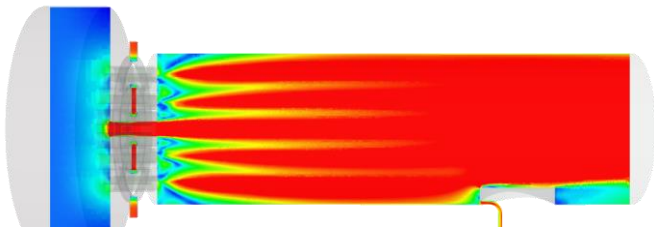


Transitioning to a Carbon-Neutral Future: A Review of Low/Zero Carbon Fuel Combustion Research at Southwest Research Institute

Brian Connolly
Research Engineer
Propulsion and Energy Machinery

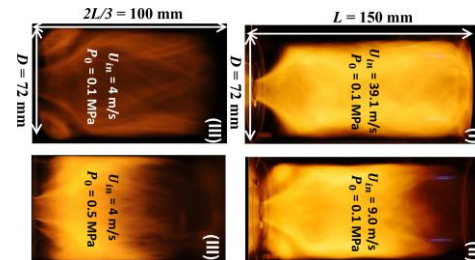
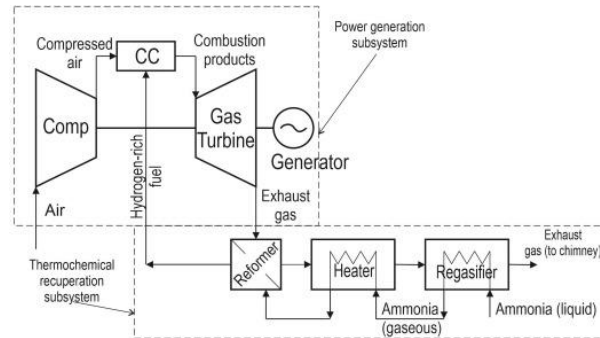
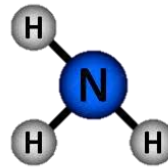
Low/Zero Carbon Fuel Combustion Activities at SwRI

Hydrogen (H₂)



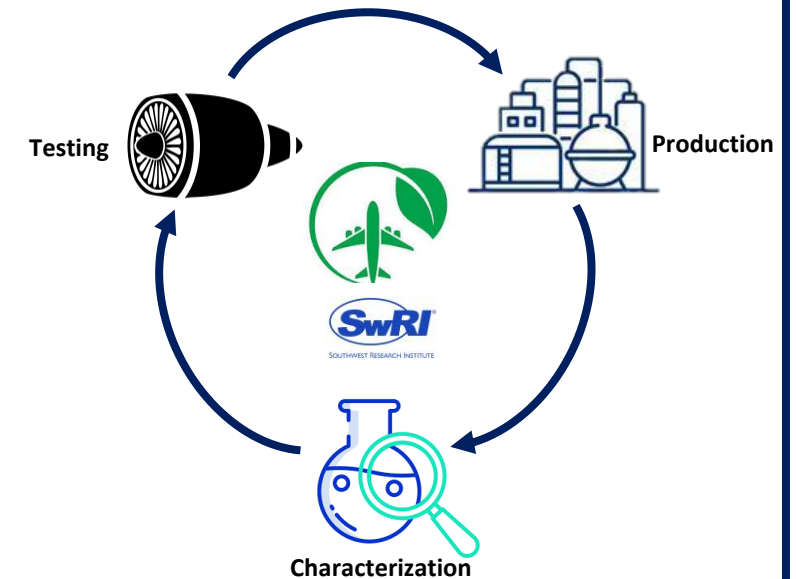
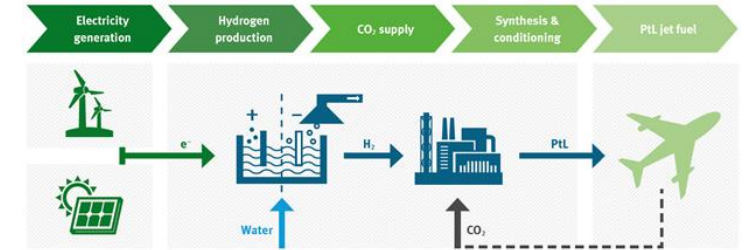
Courtesy: Dr. Tim Allison and Dr. Brian Connolly

Ammonia (NH₃)



Source: Paschenko et al., 2022, Kobayashi et al., 2019

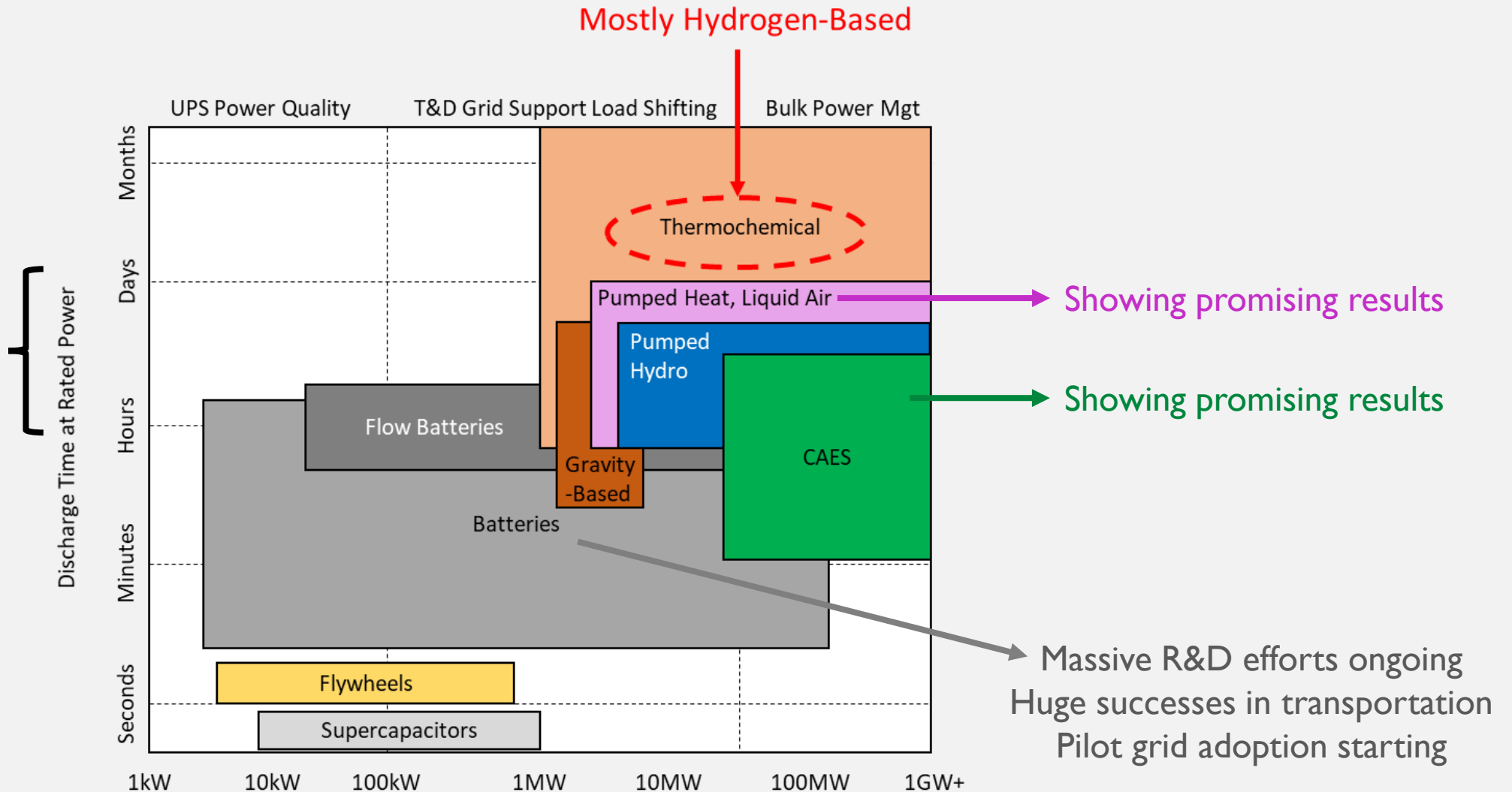
Sustainable Aviation Fuels (SAF)



Source: EESI

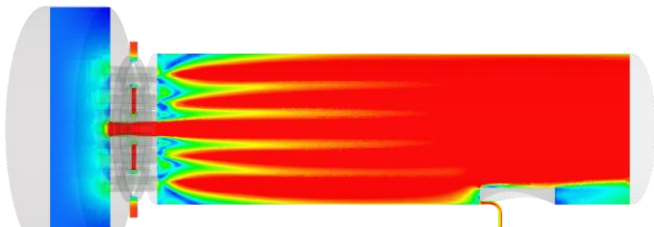
Energy Storage Landscape

Load balancing requirements for a renewables-dominated grid are typically on the order of hours to days



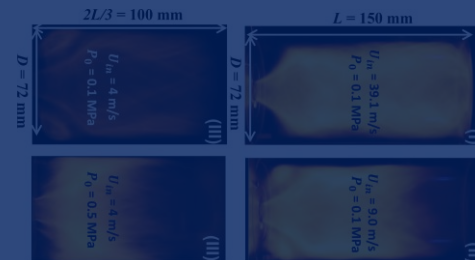
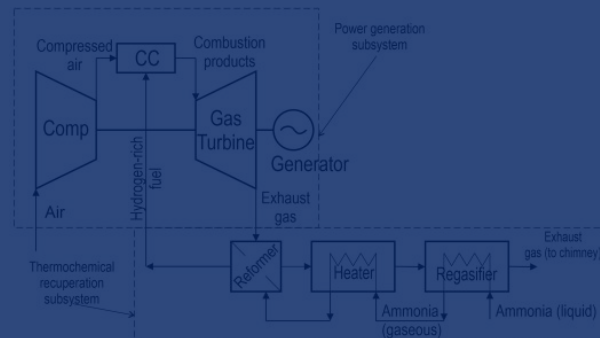
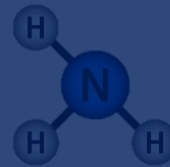
Low/Zero Carbon Fuel Combustion Activities at SwRI

Hydrogen (H_2)



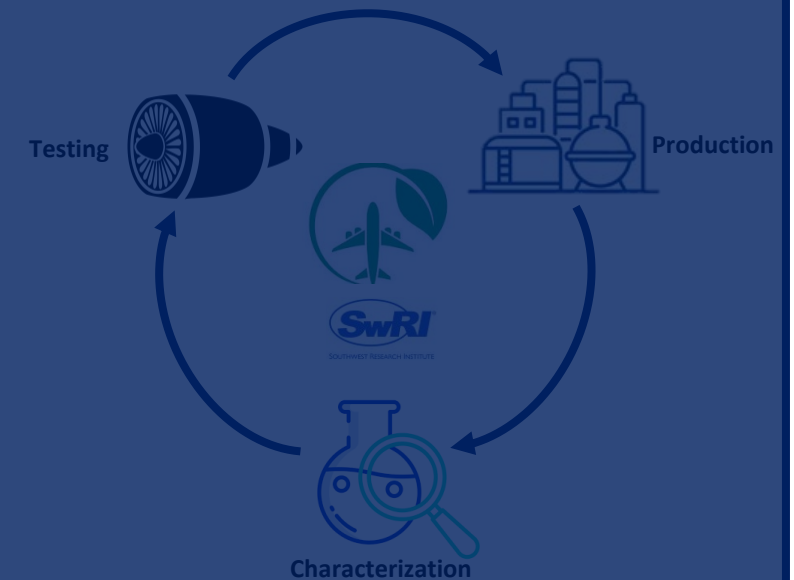
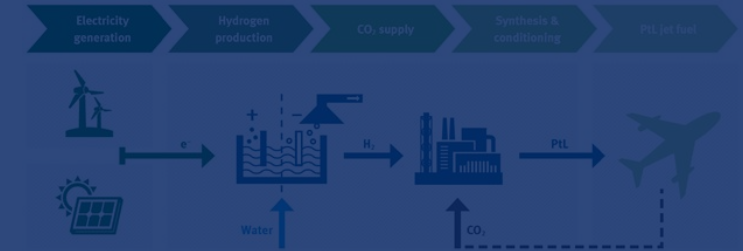
Courtesy: Dr. Tim Allison and Dr. Brian Connolly

Ammonia (NH_3)



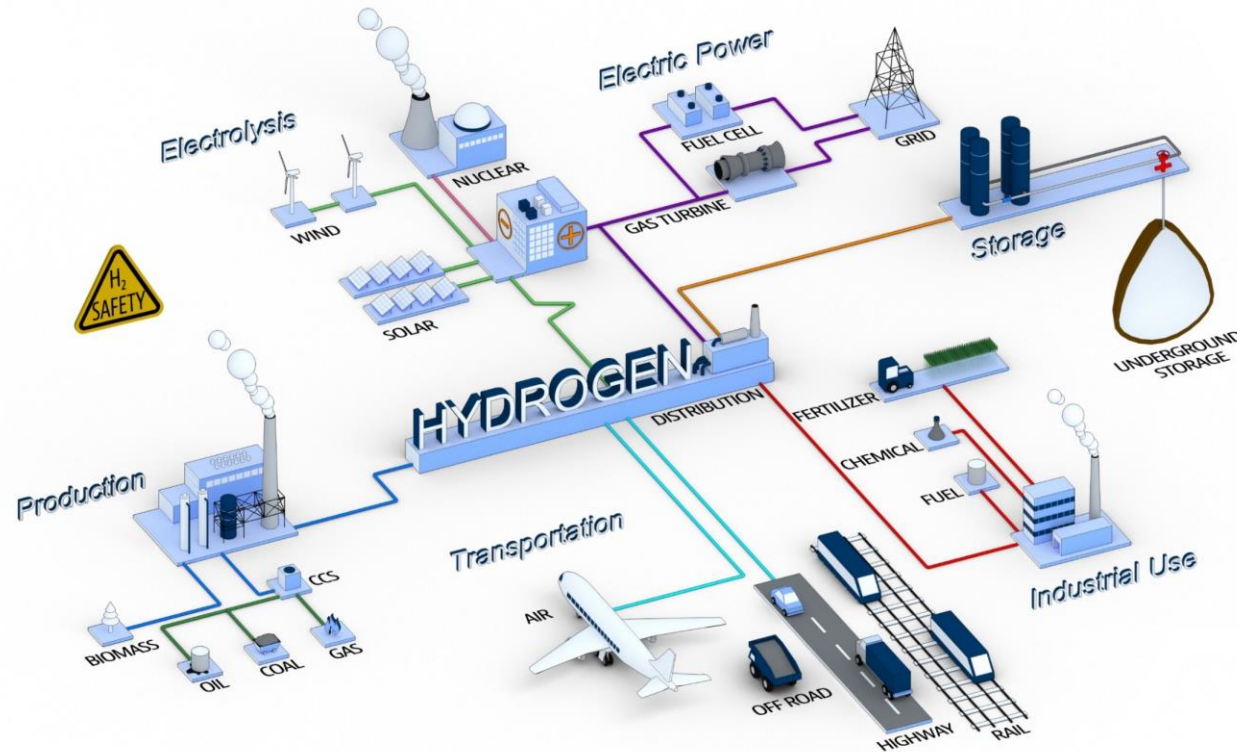
Source: Paschchenko et al., 2022, Kobayashi et al., 2019

Sustainable Aviation Fuels (SAF)



Source: EESI

Why H₂?



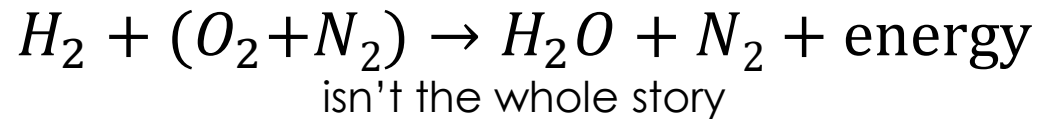
Fuel	NH ₃	H ₂	CH ₄	C ₃ H ₈
Maximum burning velocity (cm/s)	7	291	37	43
Lower calorific value (MJ/kg)	18.6	120	50	46.4
Flammability limit (in terms of Φ)	0.63-1.4	0.1-7.1	0.5-1.7	0.51-2.5
Auto-ignition temperature (K)	924	844	813	739
Adiabatic flame temperature (K)	2073	2383	2223	2273

Source: Elbaz et al, 2022

- No carbon emissions
- Easy (but expensive) to produce
- Larger flammability limits
- Highly flammable
- Difficult to reliably burn
- Difficult to transport
- Difficult to store

H₂ stable combustion is difficult to achieve

- Flashback – flame can travel upstream and briefly enter the fuel injector or fuel line
- Hot spots – poor mixing can lead to high NO_x and non-uniform combustor heating
- Volume – hydrogen requires more oxygen, so more air or oxy-fuel combustion needed
- Joule-Thomson Effect – at process temperatures, hydrogen heats when expanding

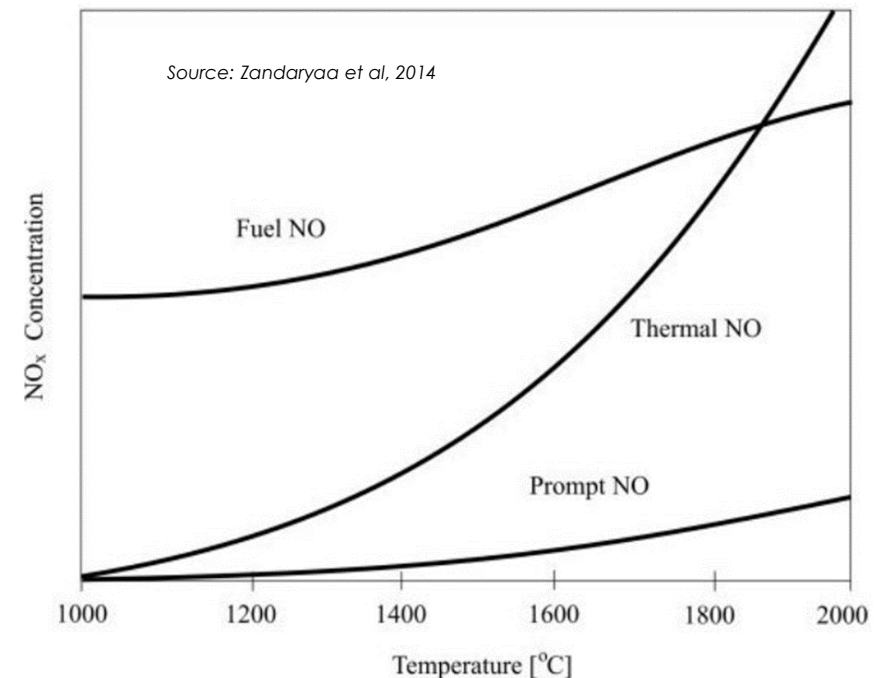


N₂ in the air dissociates

No fuel NO_x for H₂ but

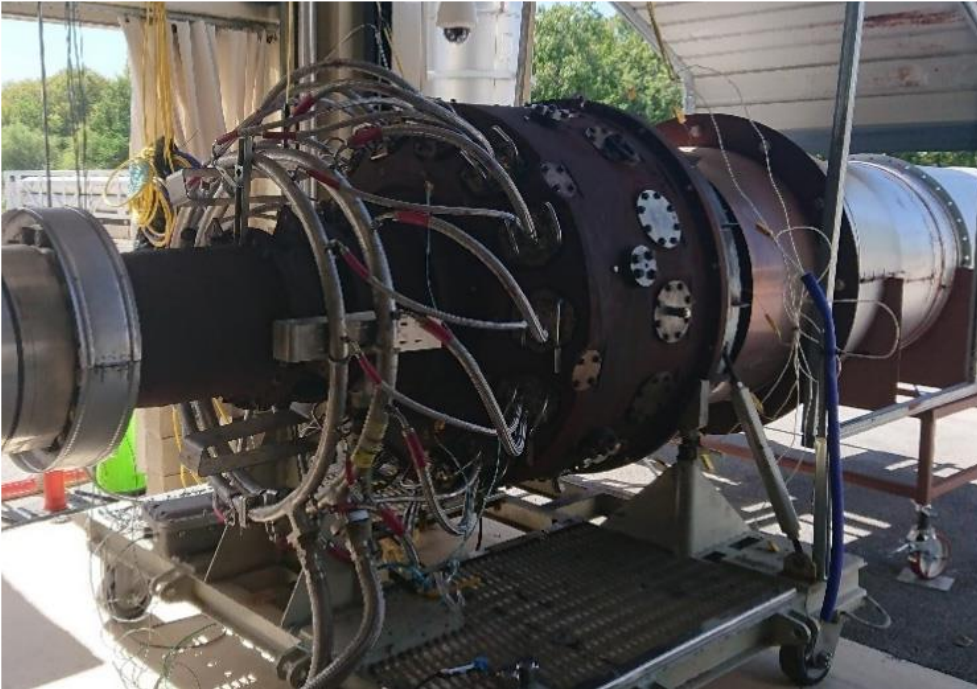
Thermal NO_x: Temperature dependent

Prompt NO_x: Reaction/Temperature dependent



H₂ combustion at SwRI

- SwRI operates a gas turbine (GT) combustion test facility to support the development of new combustion system



SwRI tested a Titan 130 SoLoNOx combustion system with CH₄/H₂ blended fuels – DE-EE0008415

The facility is design for:

$$P_{\max} = 28 \text{ barg}$$

$$T_{\max} = 800 \text{ K}$$

$$Q_{\max} \text{ air} = 6.4 \text{ kg/s}$$

$$Q_{\max} \text{ H}_2 = 0.055 \text{ kg/s}$$

H₂ combustion at SwRI

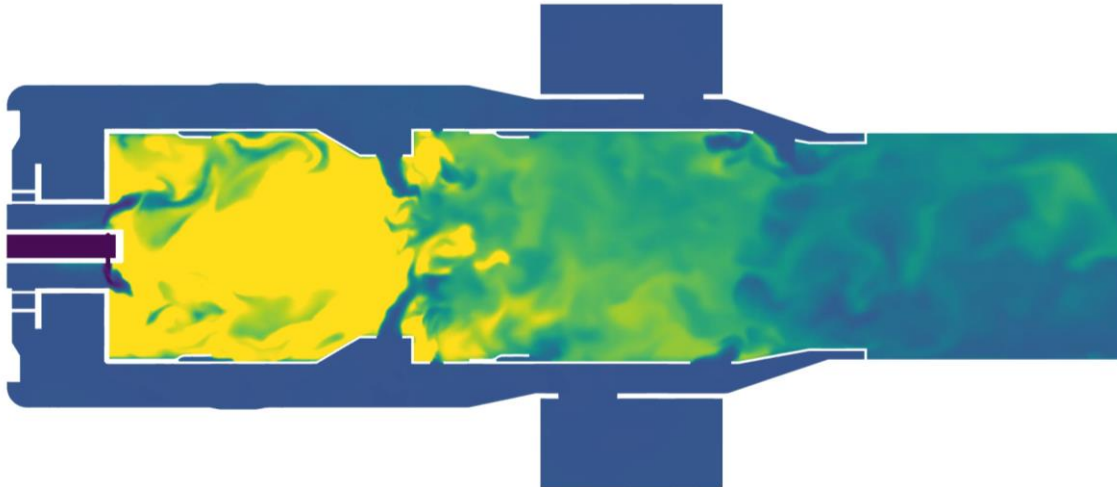


DOOSAN

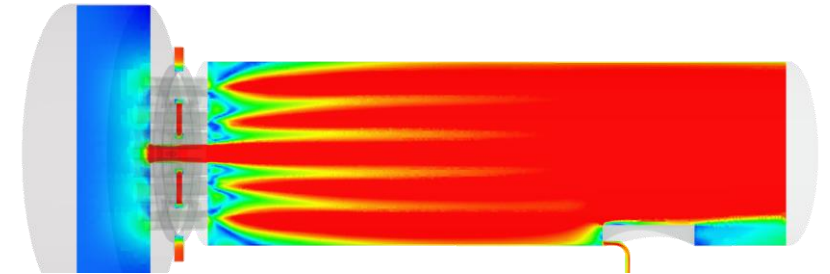


- Combustion design and simulations

TurboGen CHP Rich Quench Lean (RQL) Combustor



Doosan and Convergent Science validation of NASA partially premixed experiments



Not just H₂ combustion at SwRI

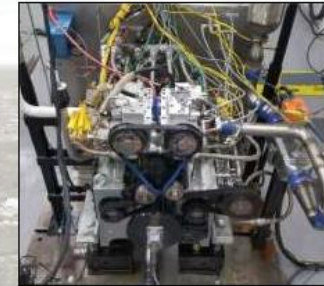
*Hydrogen
Compressor
Development
and Test Loop*



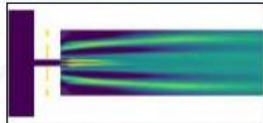
17500 Gallon LH2 Supply



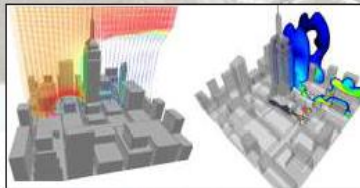
*Hydrogen
Testing in
Combustion
Engines*



*Hydrogen
Combustion
Testing and
Injector Design
for Hydrogen*

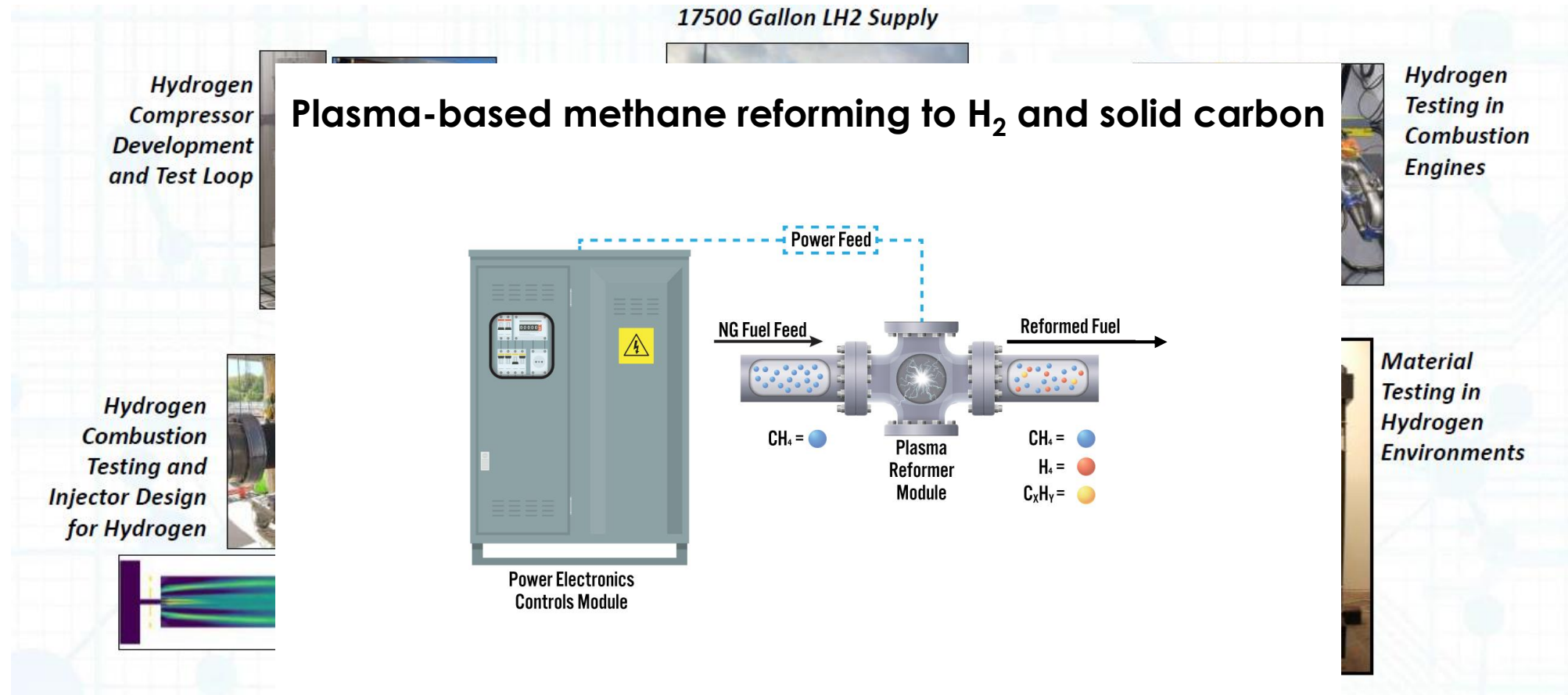


*Material
Testing in
Hydrogen
Environments*



Hazard Assessments and Leak Detection

Not just H₂ combustion at SwRI



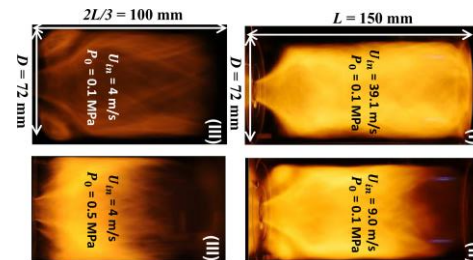
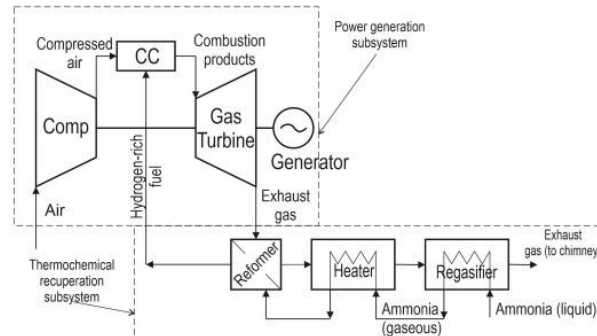
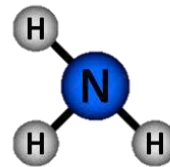
Low/Zero Carbon Fuel Combustion Activities at SwRI

Hydrogen (H₂)



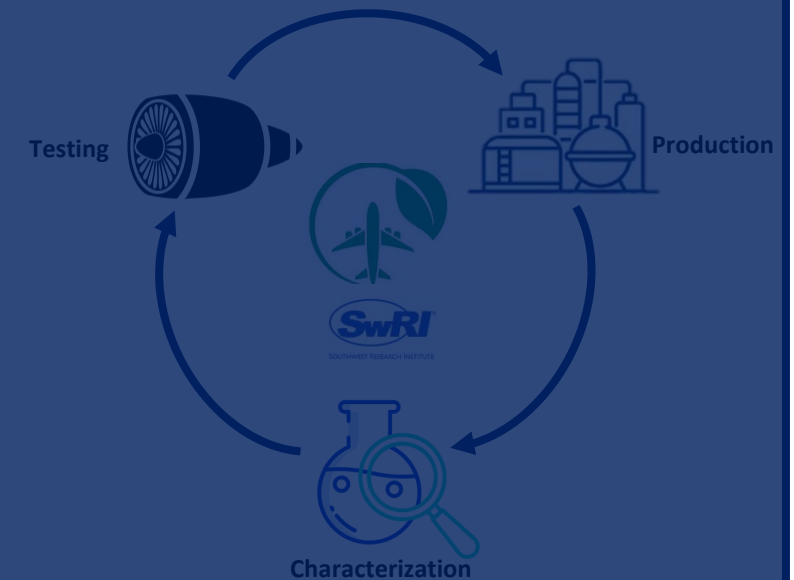
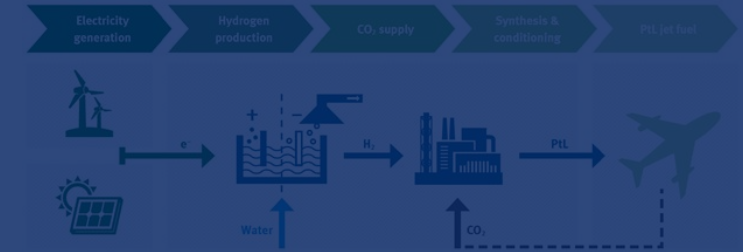
Courtesy: Dr. Tim Allison and Dr. Brian Connolly

Ammonia (NH₃)



Source: Paschchenko et al., 2022, Kobayashi et al., 2019

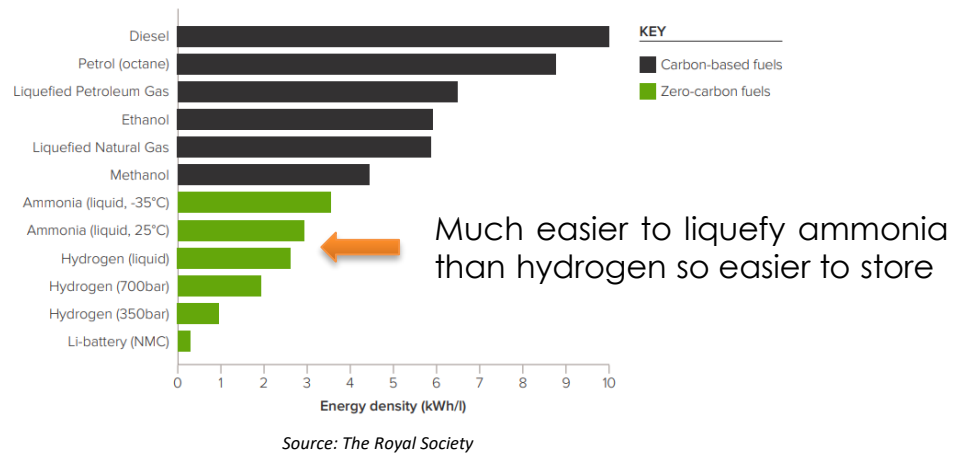
Sustainable Aviation Fuels (SAF)



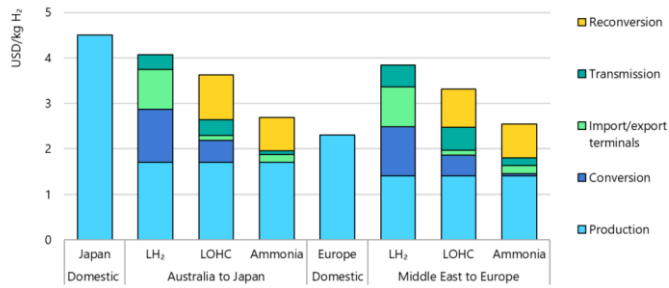
Source: EESI

Why NH₃?

- Higher volumetric energy density than H₂



- Infrastructure for production, delivery, and storage are already in place



Ammonia is and will be cheaper due to lower conversion and transmission costs

Fuel	NH ₃	H ₂	CH ₄	C ₃ H ₈
Maximum burning velocity (cm/s)	7	291	37	43
Lower calorific value (MJ/kg)	18.6	120	50	46.4
Flammability limit (in terms of Φ)	0.63-1.4	0.1-7.1	0.5-1.7	0.51-2.5
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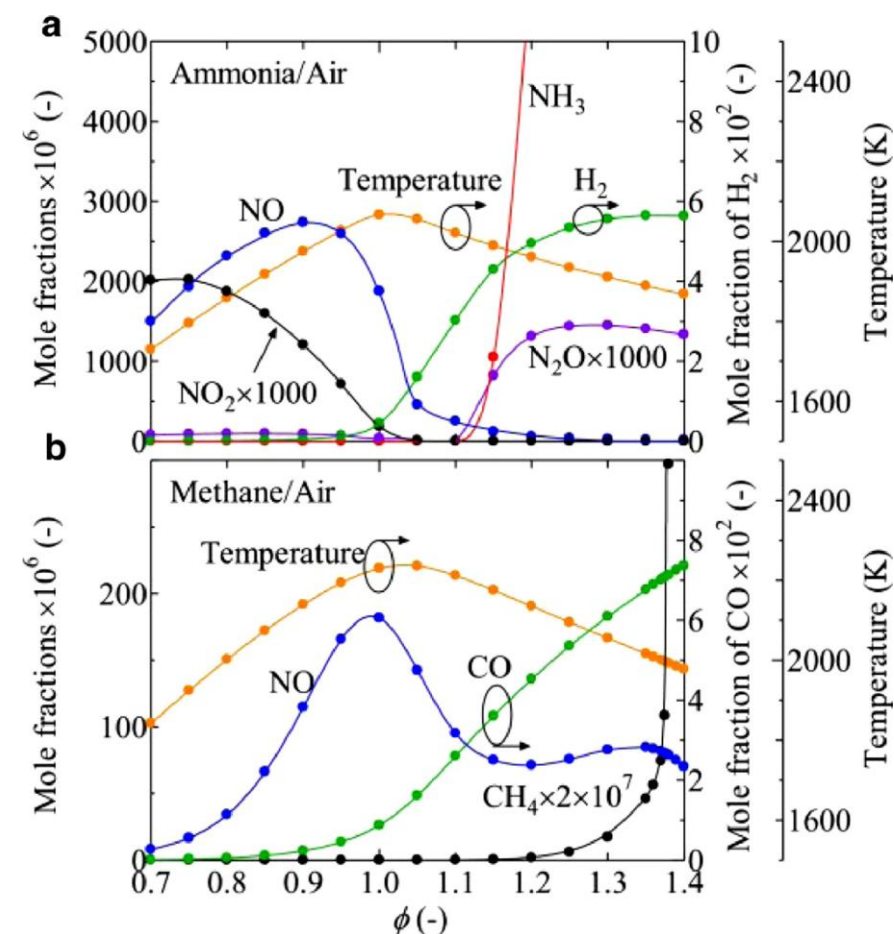
Source: Elbaz et al, 2022

- No carbon emissions
- Easy to produce
- Easy to transport
- Narrow flammability limits
- Not very flammable
- Difficult to reliably burn
- Toxic

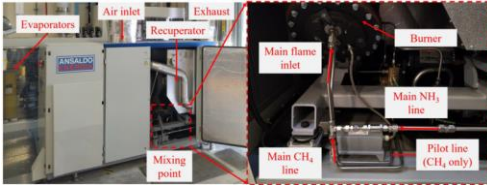
Ammonia is hard to burn efficiently and with low NOx emissions

Fuel	NH ₃	H ₂	CH ₄	C ₃ H ₈
Maximum burning velocity (cm/s)	7	291	37	43
Lower calorific value (MJ/kg)	18.6	120	50	46.4
Flammability limit (in terms of Φ)	0.63-1.4	0.1-7.1	0.5-1.7	0.51-2.5
Auto-ignition temperature (K)	924	844	813	739
Adiabatic flame temperature (K)	2073	2383	2223	2273

Overall “worse” combustion properties and higher NOx emissions than a conventional CH₄ combustor

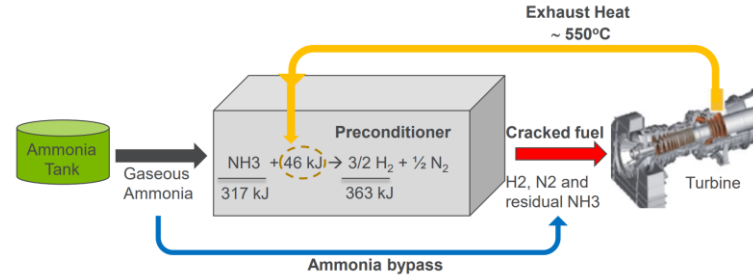


Previous and on-going work on ammonia combustion for gas turbine



Micro gas turbine powered by ammonia-methane mix (Saudi Arabia)

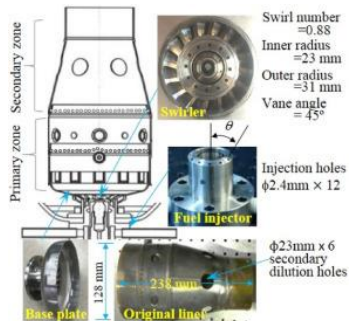
Source: Avila et al, 2023



Ammonia craked and mixed with NG
ANL + Purdue

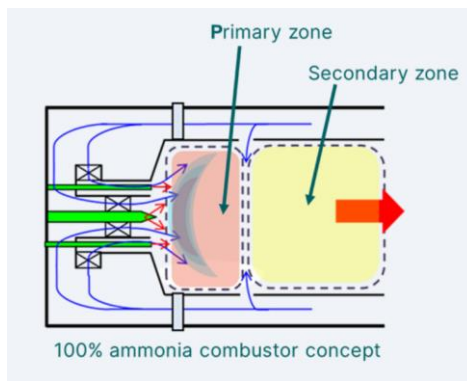
Not been demonstrated at relevant conditions

Source: Gupta et al, 2023



Gas turbine combustor powered by ammonia (Japan)

Source: Kobayashi et al, 2019



GE +IHI two stage combustor for 100% NH_3 combustion (USA + Japan)

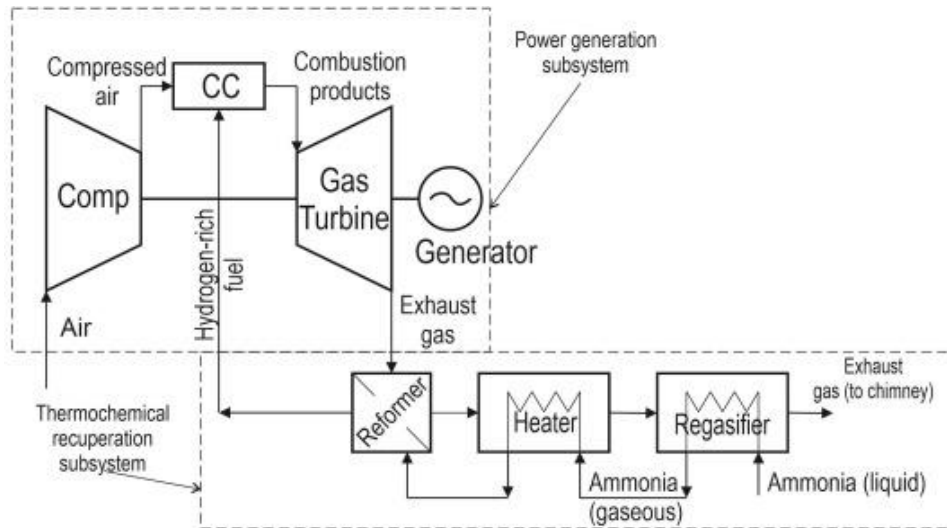
Similar approach for CPS, RTX + Uconn, GTI + UCF (USA)

Source: GE Vernova

- Dual-fuel configurations ($\text{NG} + \text{NH}_3$ or $\text{H}_2 + \text{NH}_3$)
- Direct ammonia combustion with two-stage combustors
- Ammonia craking into $\text{NH}_3 + \text{H}_2 + \text{N}_2$ (not demonstrated at relevant conditions)

Ammonia chemically recuperated gas turbine cycle

A system approach is needed to properly implement ammonia cracking in gas turbine cycles



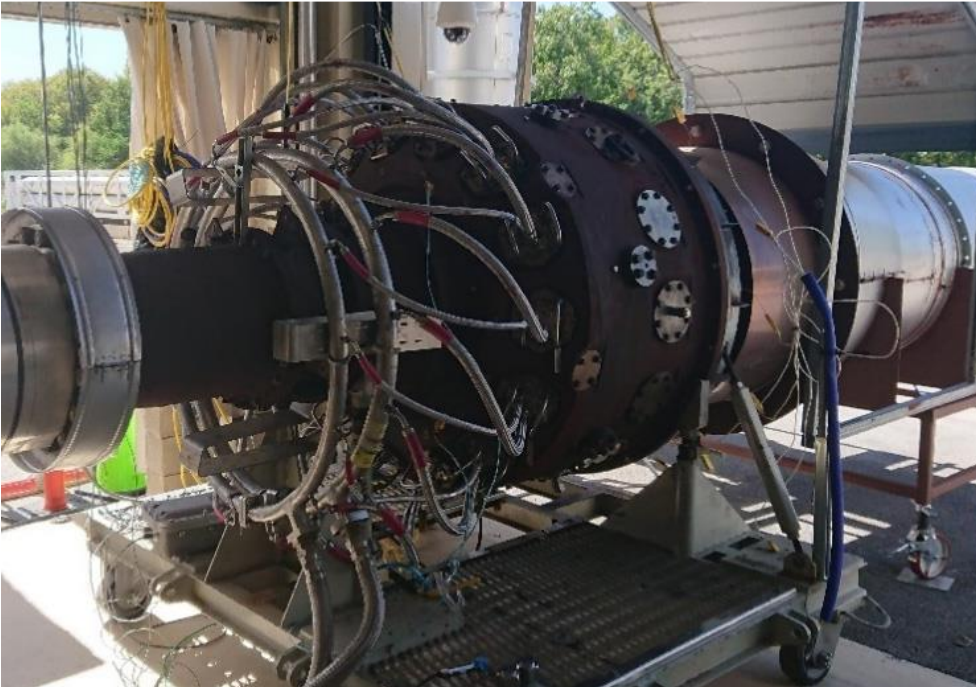
- Demonstrate that $\text{NH}_3\text{-H}_2\text{-N}_2\text{-AIR}$ combustion in the context of chemically recuperated gas turbine cycle
- Higher efficiency has been shown but not demonstrated
- Vaporization of NH_3 using exhaust gases can be useful to reduce NH_3 supply infrastructure costs



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NH₃ combustion at SwRI

- SwRI operates a gas turbine (GT) combustion test facility to support the development of new combustion system



The facility is design for:

$$P_{\max} = 28 \text{ barg}$$

$$T_{\max} = 800 \text{ K}$$

$$Q_{\max} \text{ air} = 6.4 \text{ kg/s}$$

$$Q_{\max} \text{ NH}_3 = 0.2 \text{ kg/s}$$

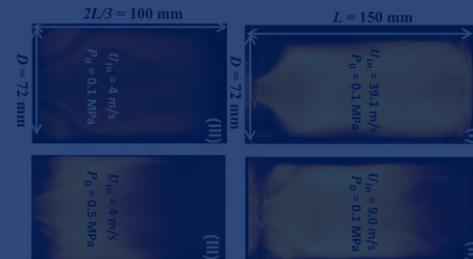
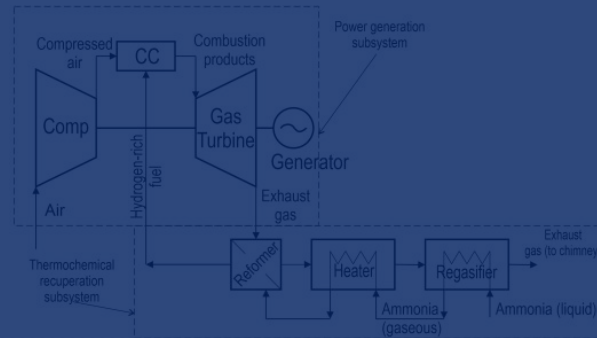
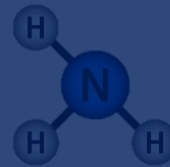
Low/Zero Carbon Fuel Combustion Activities at SwRI

Hydrogen (H_2)



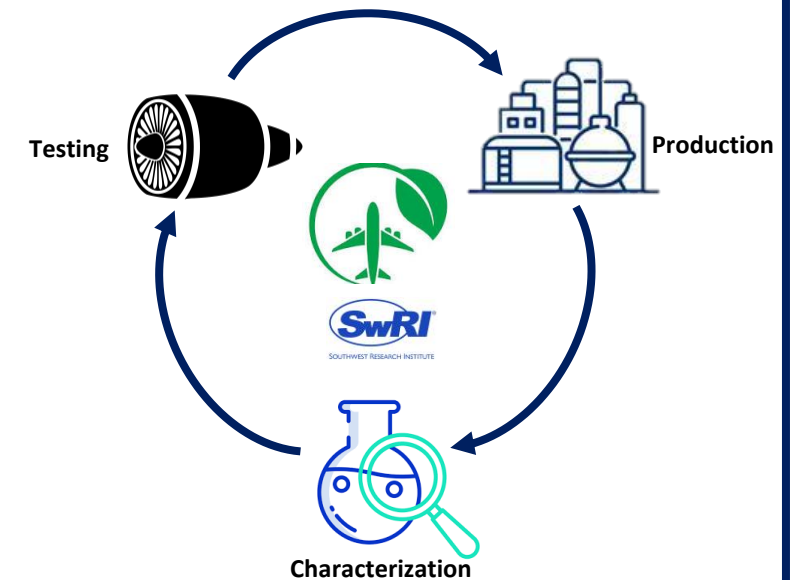
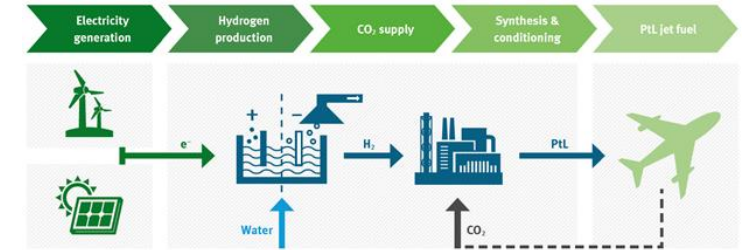
Courtesy: Dr. Tim Allison and Dr. Brian Connolly

Ammonia (NH_3)



Source: Paschchenko et al., 2022, Kobayashi et al., 2019

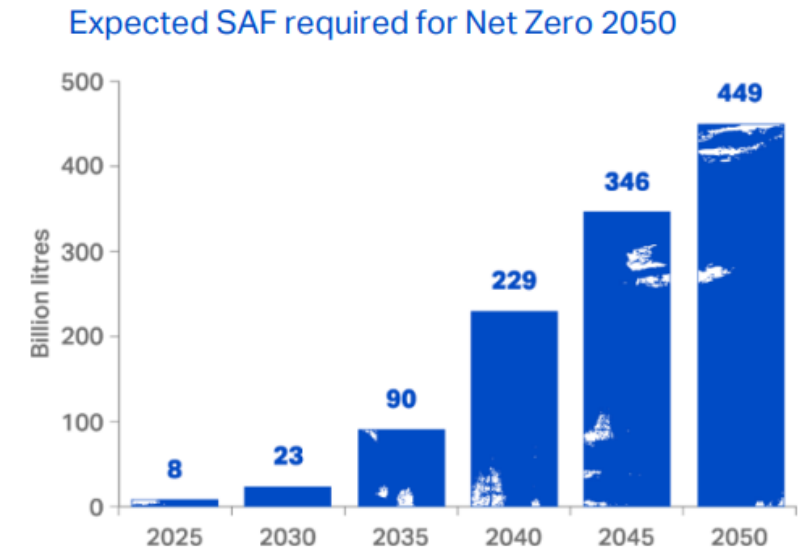
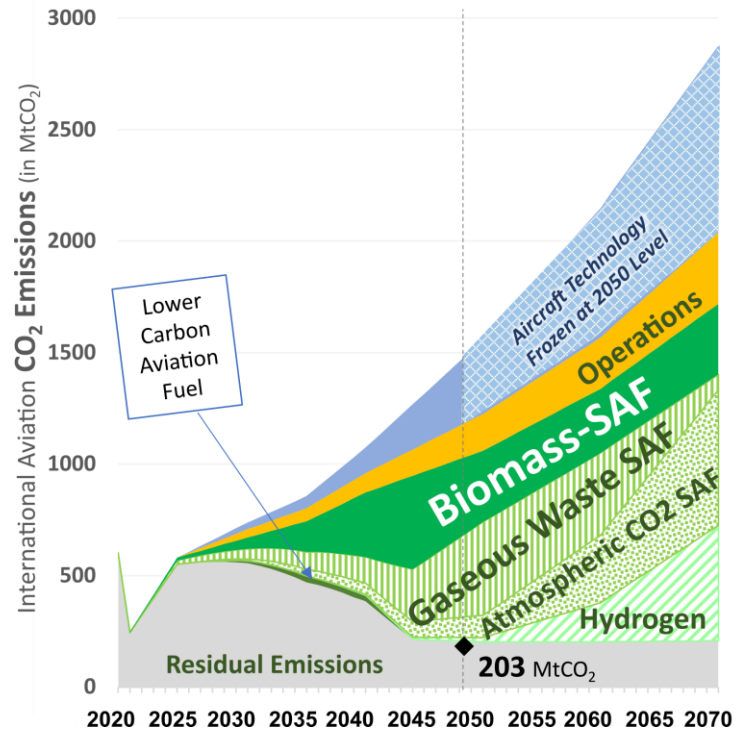
Sustainable Aviation Fuels (SAF)



Source: EESI

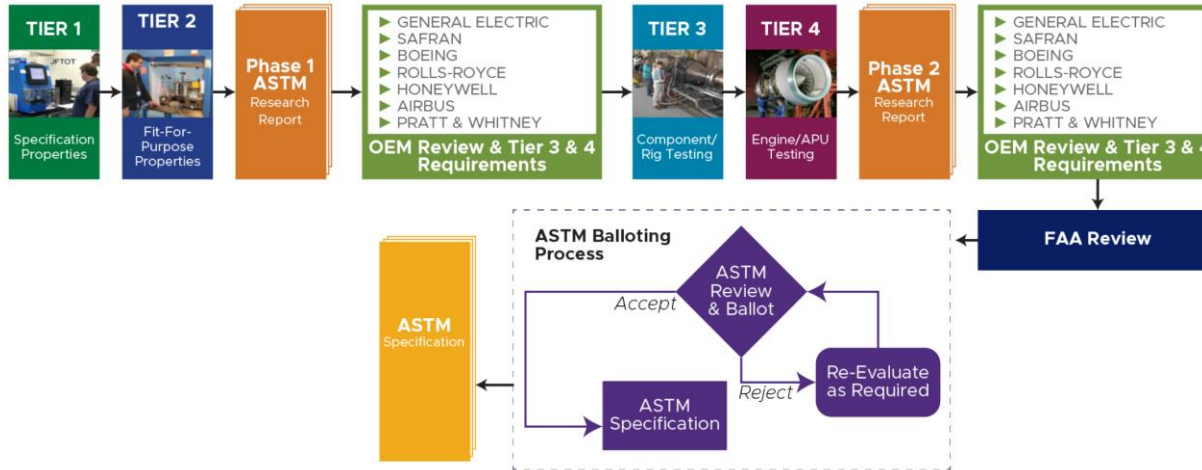
Why SAF?

A Sustainable Aviation Fuel (SAF) is a fuel for aviation with an alternative feedstock to crude oil which can reduce lifecycle emissions by up to 80% compared to conventional jet fuel.



The global SAF market was valued at \$1.1 billion in 2023, and it is projected to reach USD \$16.8 billion by 2030

SAF characterization and qualification



Before a fuel can be utilized and further tested, it must meet the ASTM D4054 standard

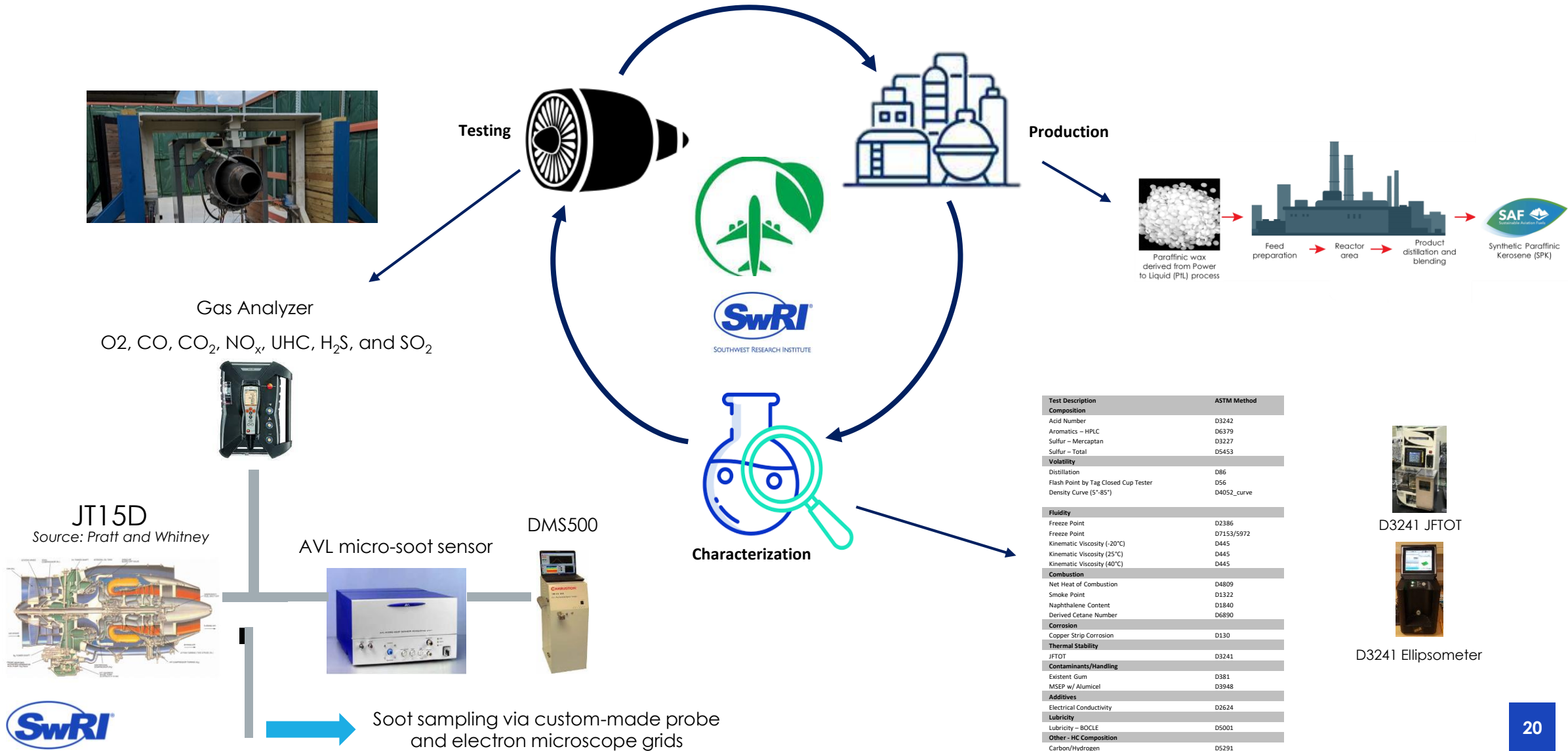
- Extremely expensive in terms of fuel, time, and money
- Still limited to 50% in volume
- Substantial research needed to move to 100%

Tier	Approximate Fuel Volume in Gallons (Liters)	Approximate Time in Months	Approximate Cost in U.S. Dollars
Tier 1 – Fuel specification properties	10 (40)	6 months	\$50,000 (testing cost)
Tier 2 – Fit-for-purpose properties	10–100 (40–400)		
OEM Review		6–12 months	\$350,000 (OEM cost)
Tier 3 – Component and rig testing	250–10,000 (950–40,000)	24–36 months	~\$4 million (testing cost)
Tier 4 – Aircraft and engine testing	Up to 225,000 (850,000)		
OEM Review and Approval		6–12 months	~\$1 million (OEM cost)

SAF production, characterization, and testing facility at



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THANK YOU FOR YOUR ATTENTION!