

# Compression Challenges for Carbon Dioxide

July 31, 2024

Robert Pelton

# Introduction

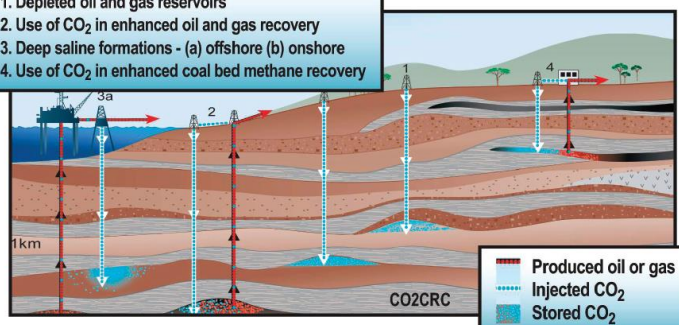
## Primary Applications for Super-Critical CO<sub>2</sub> Compression

### Carbon Sequestration

- **High Efficiency:** Its high density and low viscosity allow for better mass transfer, resulting in higher capture rates.
- **Lower Energy Consumption:** sCO<sub>2</sub> can lead to lower energy requirements for the carbon capture process
- **Reduced Footprint:** The compact nature of sCO<sub>2</sub> systems allows for smaller equipment sizes and reduced infrastructure compared to other capture technologies.
- **Versatility:** sCO<sub>2</sub> can be used in a variety of carbon capture applications, including pre-combustion, post-combustion, and oxy-fuel processes.

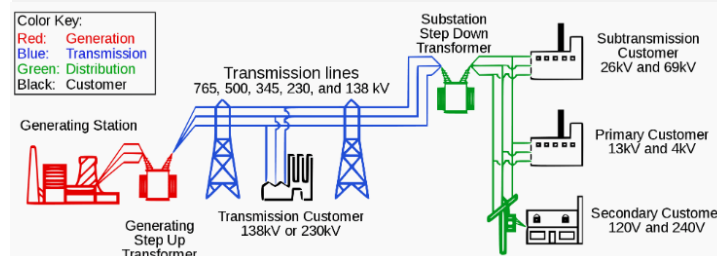
#### Overview of Geological Storage Options

1. Depleted oil and gas reservoirs
2. Use of CO<sub>2</sub> in enhanced oil and gas recovery
3. Deep saline formations - (a) offshore (b) onshore
4. Use of CO<sub>2</sub> in enhanced coal bed methane recovery



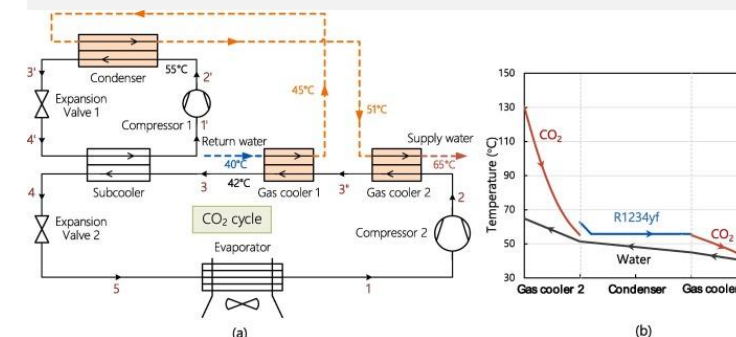
### Power Generation

- **Higher Efficiency:** sCO<sub>2</sub> power cycles operate at higher temperatures and pressures compared to steam turbines, resulting in higher thermodynamic efficiency.
- **Compact Size:** more compact than steam turbines, allowing for smaller footprint power plants. This is especially advantageous in situations where space is limited or where decentralized power generation is desired.
- **Flexibility and Load Following:** Ability to ramp up and down more quickly, making them well-suited for supporting variable renewable energy sources like wind and solar.



### Heat Pumps

- **Efficiency:** Ability to operate at high pressures and temperatures, which allows for efficient heat transfer, resulting in lower energy consumption.
- **High Temperature Capability:** One of the advantages of sCO<sub>2</sub> is its ability to reach high temperatures, making it suitable for industrial applications where high-temperature heat is required, such as in industrial processes or power generation.
- **Compact Design:** compact making them suitable for installations where space is limited. a natural refrigerant with low global warming potential (GWP) and zero ozone depletion potential (ODP).



# Introduction

## Compression Equipment Configurations

### Beam Style

- **Low Maintenance Requirements:** The design of integrally geared compressors typically results in lower maintenance requirements.
- **High Reliability:** Robust configuration with minimal seals, minimal bearings, and low dynamic pressures makes for a robust design at high pressures.
- **High Efficiency at High Flow Rates:** Centrifugal barrel compressors are highly efficient at handling high flow rates. They can effectively compress large volumes of gas to moderate pressures with relatively low energy consumption.



### Integrally Geared

- **Modular Design:** These compressors feature a modular design with multiple compressor stages driven by individual gears. This modular construction allows for flexibility in configuration and scalability.
- **Inter-cooling:** Ability to inter-cool each stage allows the ability to reduce power consumption by approaching.
- **Compact Footprint:** Despite their high capacity and performance, integrally geared compressors have a relatively compact footprint compared to other types of compressors with similar capabilities.



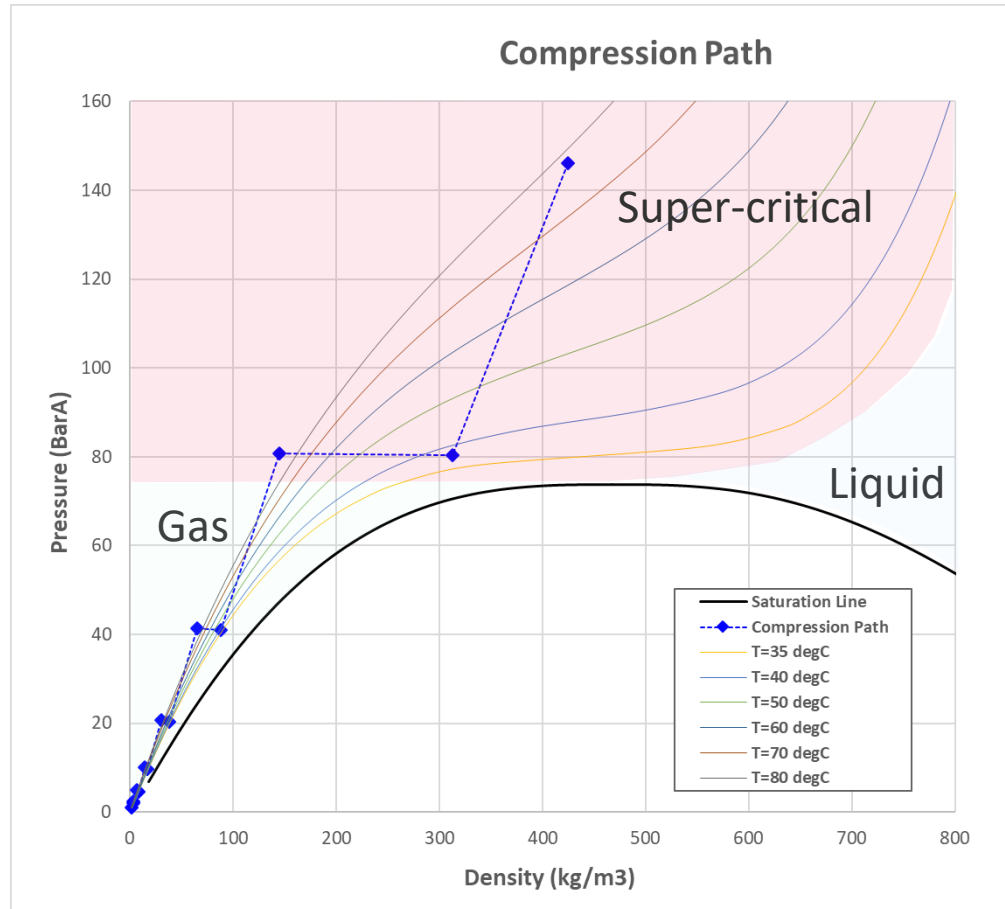
### Reciprocating

- **High Compression Ratios:** Reciprocating compressors are capable of achieving high compression ratios, making them suitable for applications requiring high-pressure delivery.
- **Cost-effectiveness for Small to Medium Applications:** Generally more cost-effective for small/medium applications. They have lower initial capital costs and are simpler in design.
- **Efficiency at Low Flow Rates:** Reciprocating compressors excel at handling low flow rates efficiently. Suitable for applications where variable demand is common or where the compressor needs to operate at different flow rates.



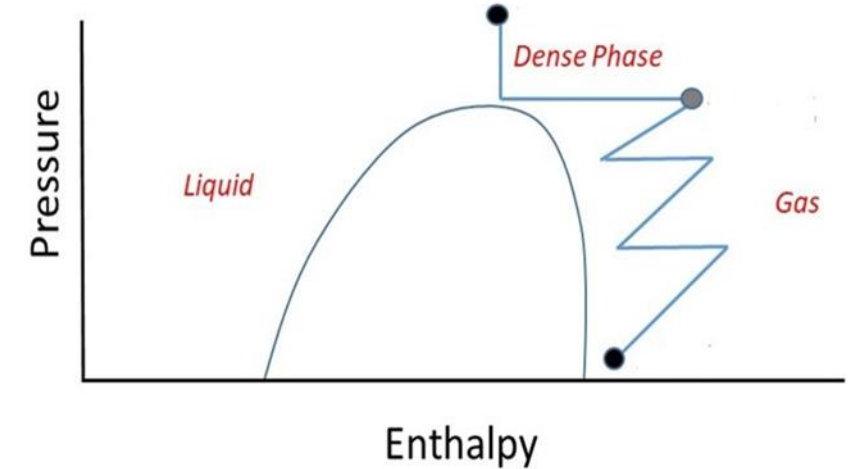
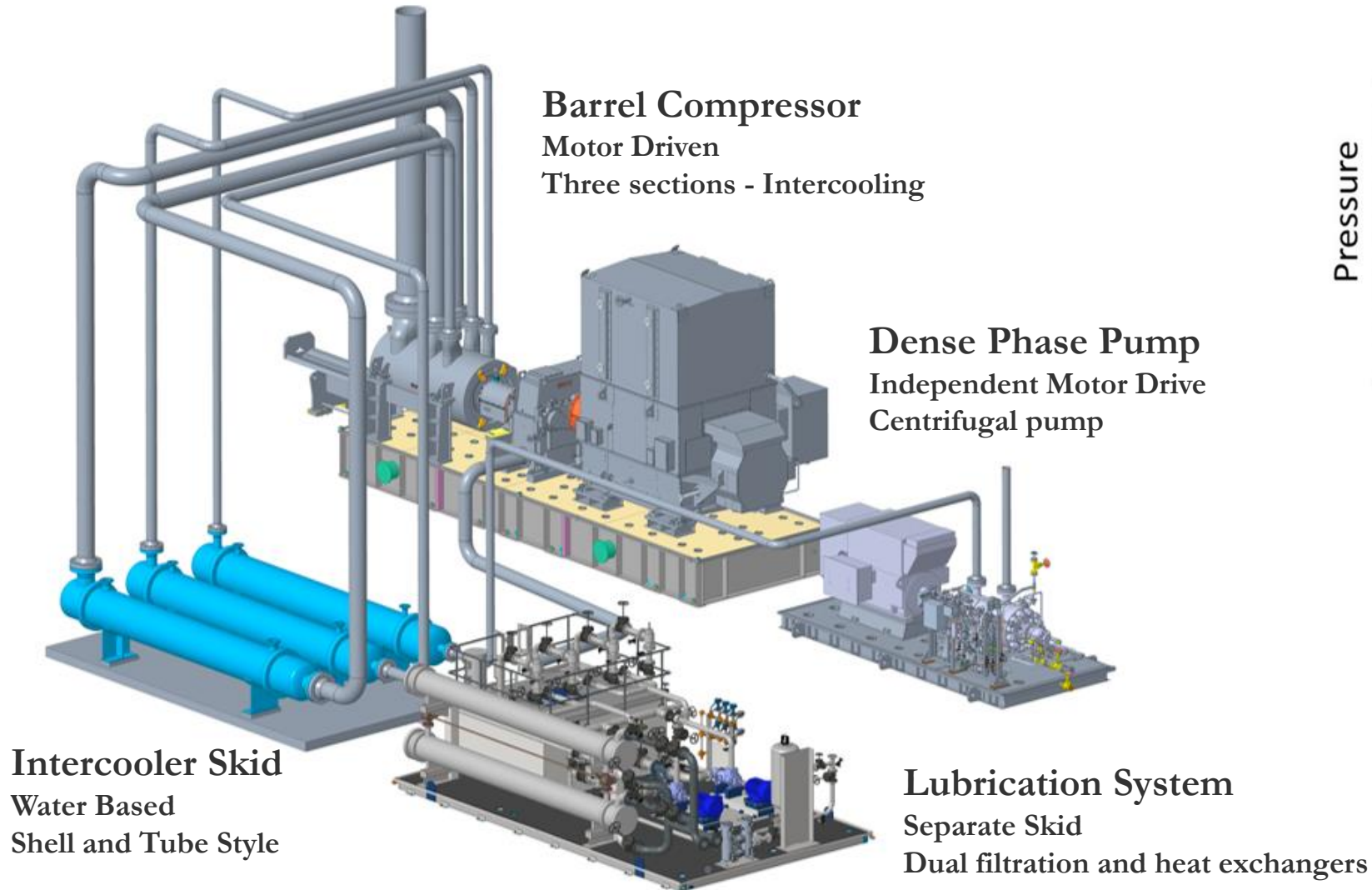
# CO2 Sequestration

## Compression Process Overview



- Compressors achieve a **pressure ratio of 145:1** in 7 stages.
- **250x increase in gas density** across the machine
  - The first 5 stages operate sub-critical in the gas region
  - The last 2 stages operate at super-critical pressure and real gas effects are pronounced and strongly impact performance
- Substantial reduction in stage size though the machine.
  - Stage 1 = 31"dia → Stage 7 = 4.75" diameter
  - Stage matching is very dependent on intercooling.
- **Extreme levels of power density** are generated in the super-critical stages.
  - 7,000kJ of energy added to ever cubic meter of flow in the 7<sup>th</sup> stage compared to just 100kJ/m<sup>3</sup> for the first stage
  - Aero and mechanical design work must be closely coupled

# Compression and Dense Phase Pump Solution for CO<sub>2</sub> Sequestration

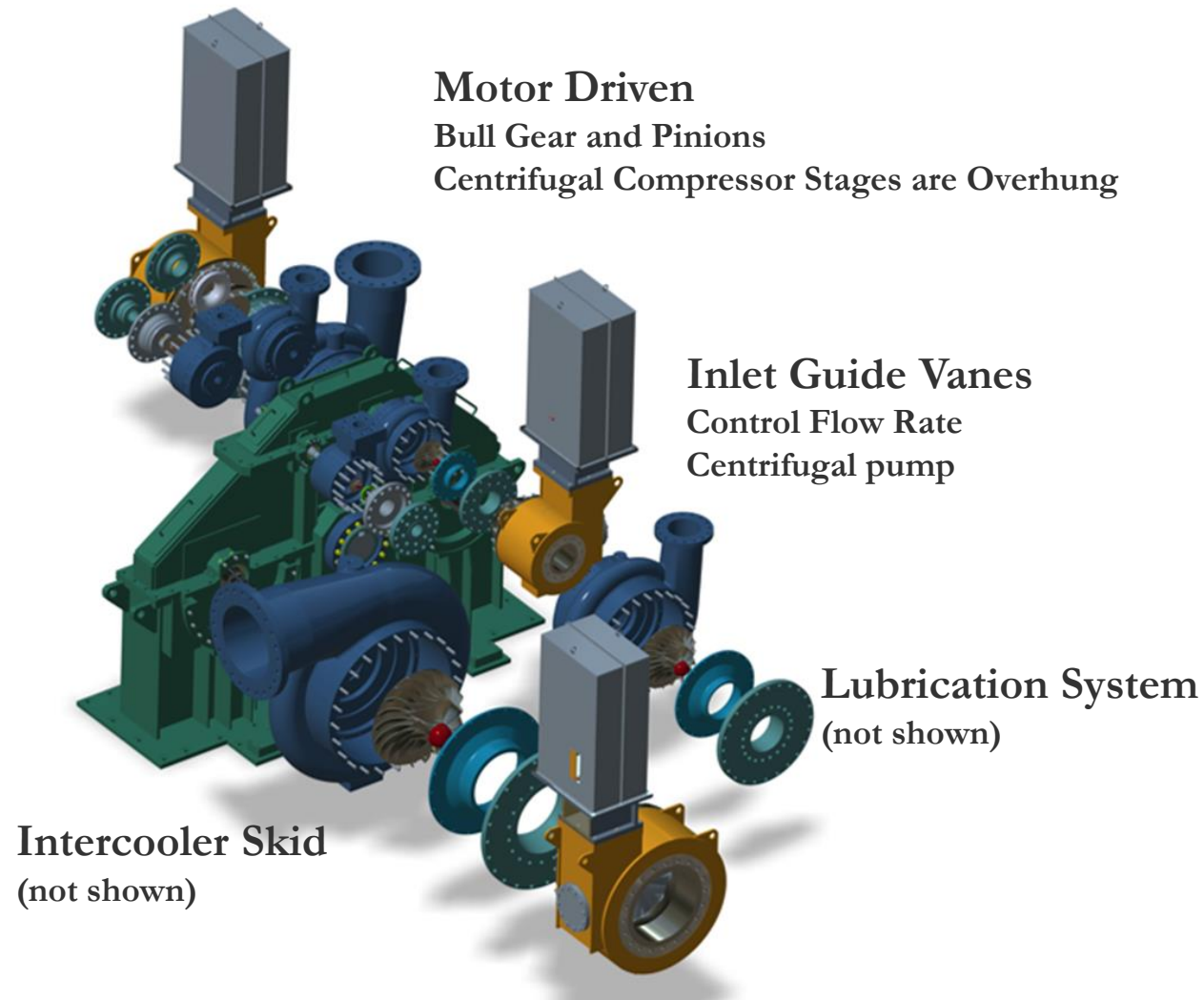


## CO<sub>2</sub> Sequestration

Highly reliable process to raise CO<sub>2</sub> to dense phase.

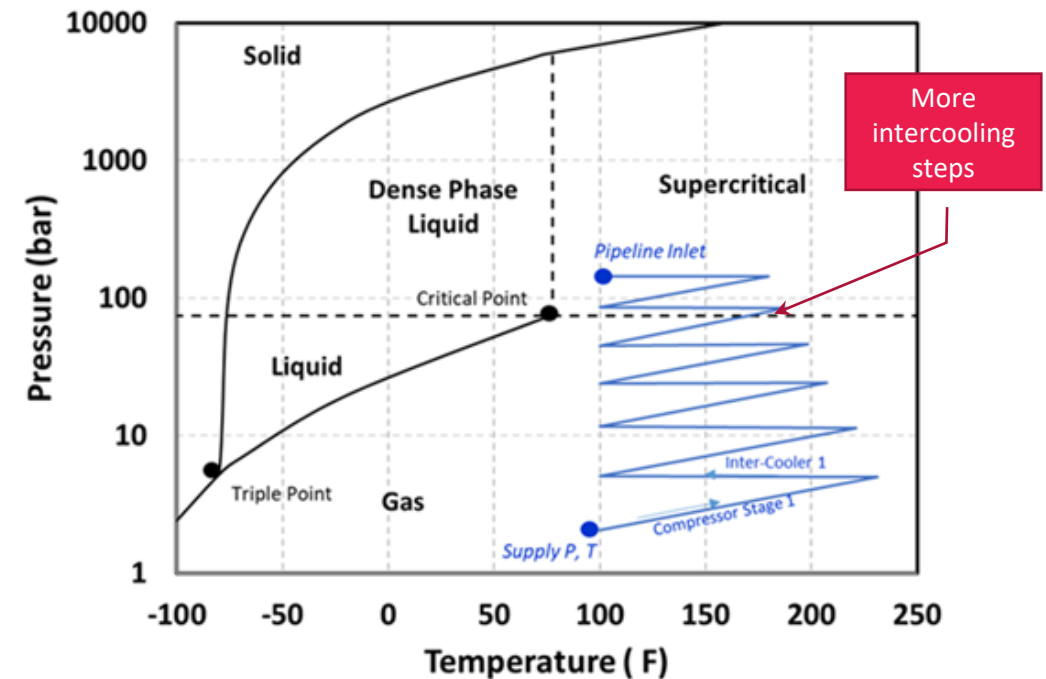


# Integrally Geared Compressor for CO<sub>2</sub> Sequestration



## CO<sub>2</sub> Sequestration

- Integrally geared compressor offers efficient method of raising pressure from atmospheric pressure to pipeline conditions.
- Inter-cooling stages reduced the power consumption of the overall package.



# Compression Options for MW Scales

|                                                        | Integrally Geared Compressor                                                                                                                                                                                                                                                                | Beam Style Compressor                                                                                                                                                                                                                                     |
|--------------------------------------------------------|---------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|-----------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------------|
| Open Loop Systems<br>(Sequestration)                   | <b>OPEX:</b> Simple integration of stage intercooling to reduce power consumption                                                                                                                                                                                                           | <b>Reliability:</b> Reduced number of gas seal points is advantage for barrel configuration.                                                                                                                                                              |
| Closed Loop Systems<br>(Power Generation & Heat Pumps) | <b>Modularity:</b> over-hung stages allow ability to quickly adjust design in development or test stand.<br><br><b>Wide Operating Range:</b> ability to apply range extension technologies.<br><br><b>Expander Stage Integration:</b> Can integrate expander.<br><br>Good for 2-25 MW (WHR) | <b>Mature Technology:</b> for high-pressures.<br><br><b>Hermetic Seal Potential:</b> Ability to seal against lower pressures.<br><br><b>Mechanical Losses:</b> fewer number of bearings and reduced losses.<br><br>Good for 10-200 MW (Nuclear/Power Gen) |

# Technology/Risk Areas to Address

|                                                        | Integrally Geared Compressor                                                                              | Beam Style Compressor                                                                             |
|--------------------------------------------------------|-----------------------------------------------------------------------------------------------------------|---------------------------------------------------------------------------------------------------|
| Open Loop Systems<br>(Sequestration)                   | Mature Technology.<br><br>Seal Improvements for Leakage.                                                  | Commercially accepted technology in O&G markets<br><br>CAPEX and OPEX tend to be higher than IGC. |
| Closed Loop Systems<br>(Power Generation & Heat Pumps) | Seal Improvements for improve reliability and leakage reduction.<br><br>Limited data near critical point. | Gas Bearings/ Magnetic Bearing for seal-less systems.<br><br>Limited data near critical point.    |



- Challenge in **Sequestration systems** is managing the change in gas density.
- Challenge in **Closed Loop Systems** is managing leakage flow:
  - Hermetically sealed systems (gas or magnetic bearings)
  - Non-hermetically sealed systems (seal leakage and recovery)
- A general challenge is **managing performance and operability** of the cycle with stages operating near the dome.

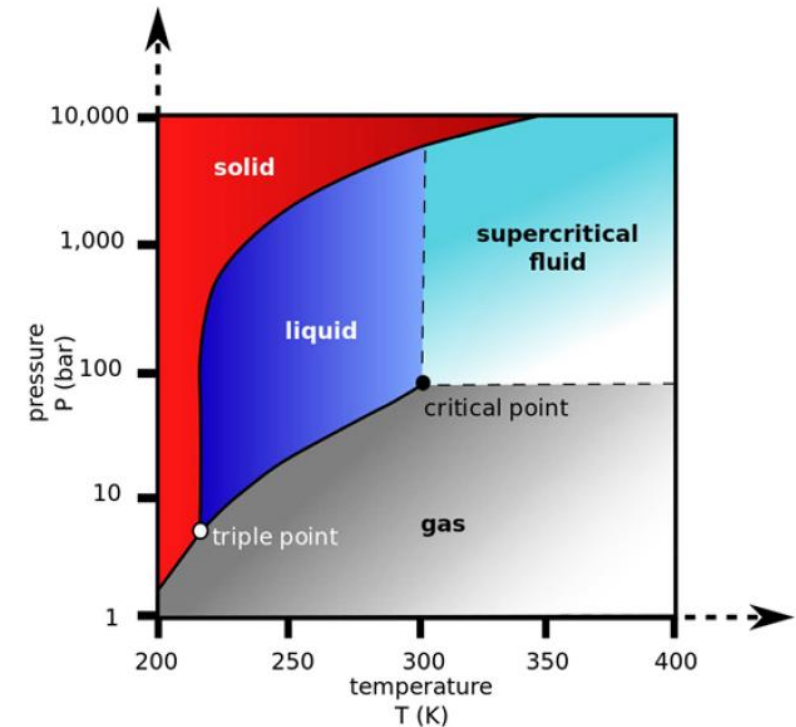
# Material Considerations for Carbon Dioxide Compression and Storage

Derrick Bauer

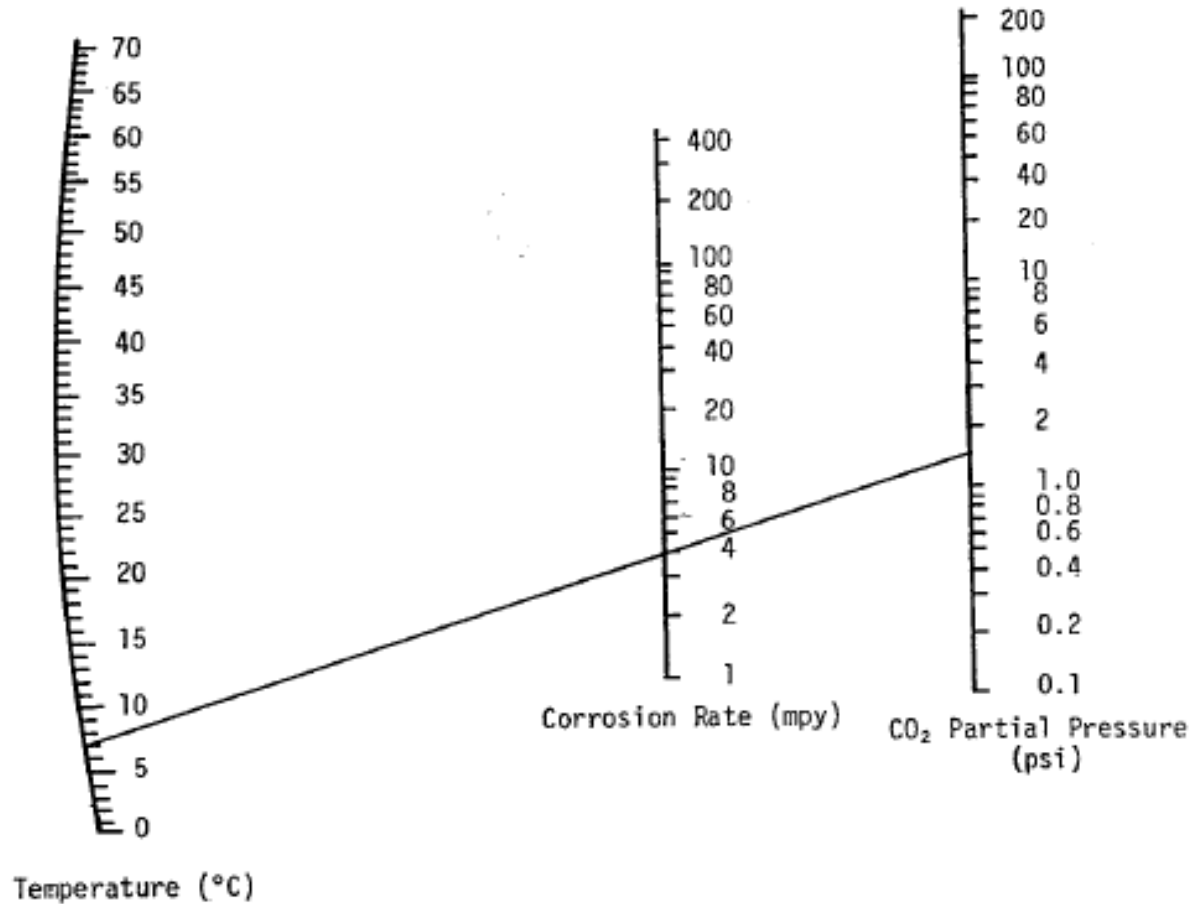
July 31, 2024

# Carbon Dioxide Storage

- Stored as a compressed gas or liquid
  - Material must be suitable for process temperature
- Corrosion
  - Dry CO<sub>2</sub> is not corrosive to steel
    - Carbon steel has been successfully utilized
  - Wet CO<sub>2</sub>
    - Forms carbonic acid, highly corrosive to carbon and low alloy steels
    - 300 series stainless steels must be utilized
    - 13%Cr-4%Ni stainless steel (CA6NM) has been successfully utilized for wet CO<sub>2</sub> applications



# CO<sub>2</sub> Corrosion Rate on Carbon Steel



Source:

Corrosion Due to Use of Carbon Dioxide For Enhanced Oil Recovery, DeBerry, D. W., Clark, W. S. 1979

CO<sub>2</sub> Corrosion in Oil and Gas Production – Selected Papers, Abstracts and References

NACE Task Group T-1-3

# How much water makes CO<sub>2</sub> “wet”

**Table 4-1 Indicative limits on maximum water content**

| <i>Reference</i>                                                        | <i>Maximum water content</i> |           |        |            | <i>Source of CO<sub>2</sub></i> |
|-------------------------------------------------------------------------|------------------------------|-----------|--------|------------|---------------------------------|
|                                                                         | [lb/MMScf]                   | [ppmW]    | [ppmV] | [ppm/Mol%] |                                 |
| Mohitpour, Golshan and Murray, 2006                                     | 18 - 30                      | 157 - 261 |        |            | -                               |
| Kinder Morgan, 2020                                                     | 30                           | 261       |        |            | CO <sub>2</sub> reservoir       |
| Equinor operated Snøhvit                                                |                              |           | 50     |            | CH <sub>4</sub> + stream        |
| Dynamis CO <sub>2</sub> quality recommendations, De Visser et al., 2008 |                              |           |        | 500        | CCS                             |

Source: DNV DNV-RP-F104

- DNV DNV-RP-J202
  - Provides recommended materials.
  - Temperature is only considered for temperatures below 400°C (750°F)

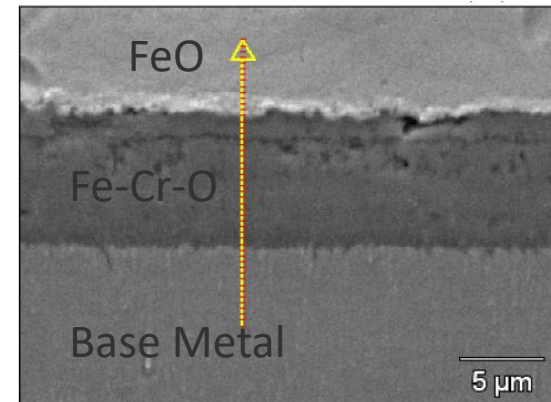
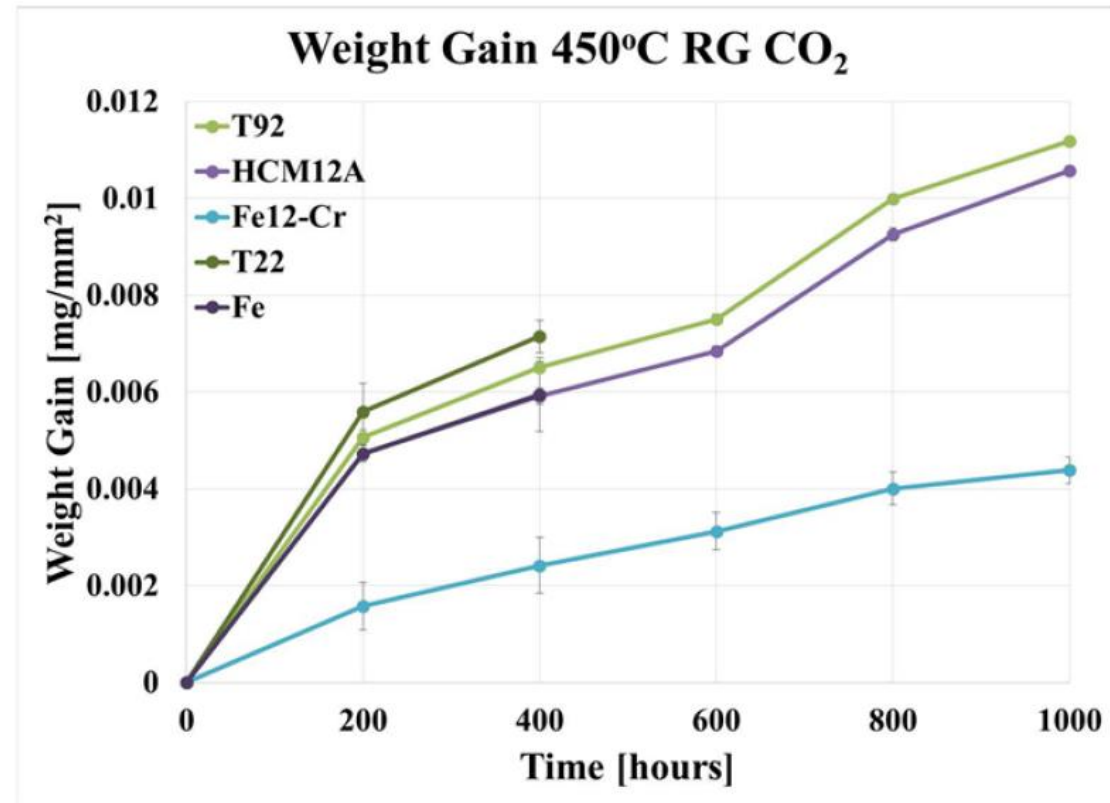
**Table 5-1 Candidate material types compatible with dense and vapour CO<sub>2</sub>**

|                       | <i>No free water</i> |                                    | <i>With free water</i> |                                    |
|-----------------------|----------------------|------------------------------------|------------------------|------------------------------------|
| Material types        | Pure CO <sub>2</sub> | CO <sub>2</sub> + H <sub>2</sub> S | Pure CO <sub>2</sub>   | CO <sub>2</sub> + H <sub>2</sub> S |
| C-and low alloy steel | ●                    | ●                                  |                        |                                    |
| 304                   | ●                    | ●                                  | ●                      | ●                                  |
| 316                   | ●                    | ●                                  | ●                      | ●                                  |
| 13Cr                  | ●                    | (●)                                | ●                      | (●)                                |
| 22Cr (duplex)         | ●                    | (●)                                | ●                      | (●)                                |
| 25Cr (duplex)         | ●                    | (●)                                | ●                      | (●)                                |
| Nickel based alloys   | ●                    | ●                                  | ●                      | ●                                  |



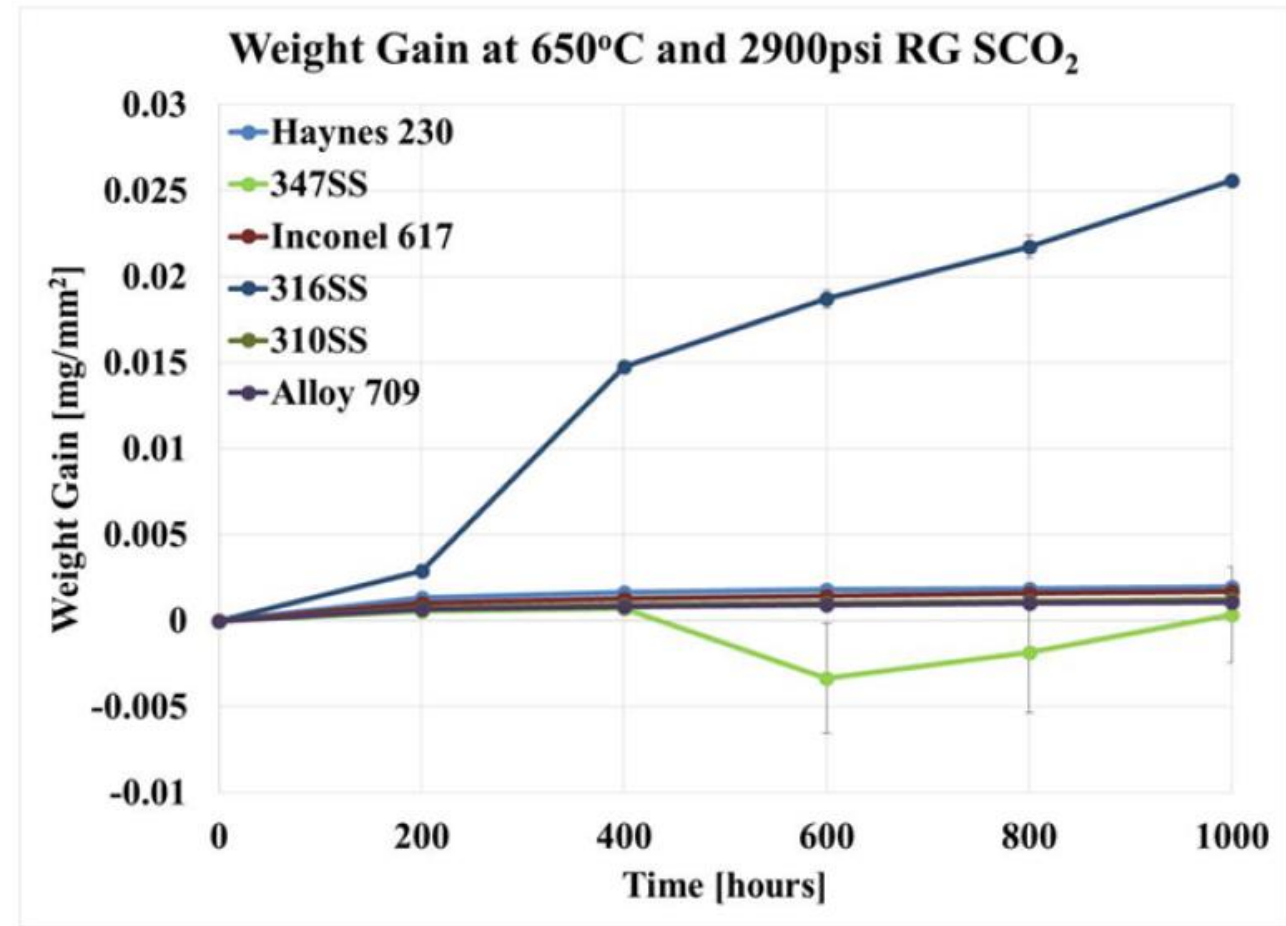
# Corrosion Testing in CO<sub>2</sub> Atmospheres

- Conditions
  - 2900 psi (20 MPa)
  - 3 ppm H<sub>2</sub>O
- 12%Cr stainless steel performed best compared to lower alloy materials
- All non-stainless steels experience oxide layer formation

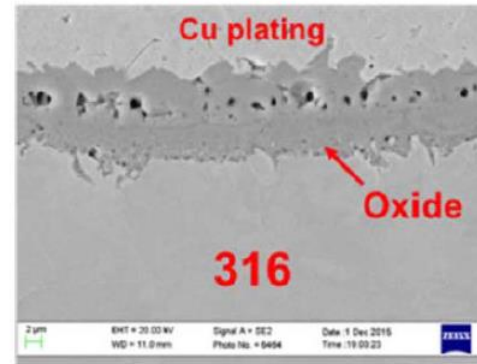


# Higher Temperature CO<sub>2</sub> Applications

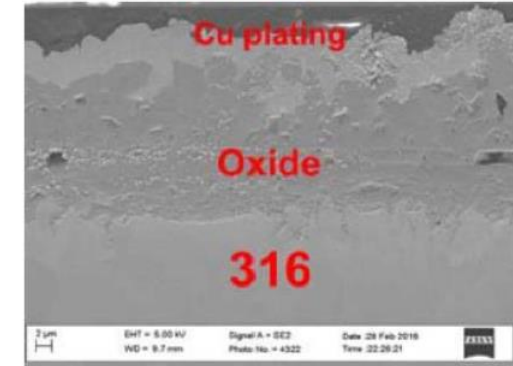
- Conditions
  - 2900 psi (20 MPa)
  - 3 ppm H<sub>2</sub>O
  - 650°C (1200°F)
- Nickel based alloys showed best resistance to corrosion
- Impurities can result in significant changes to corrosion rates



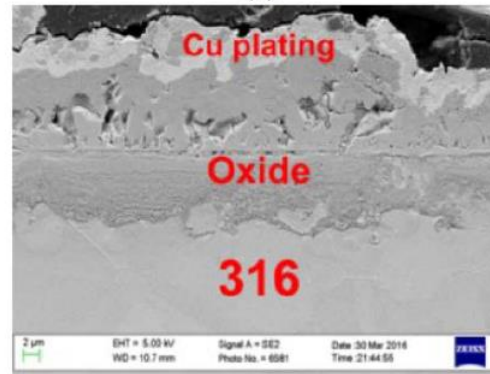
- Oxidation of 316 stainless steel at 650°C
- Sensitization of austenitic stainless steels at temperatures above 425°C (800°F) also must be considered over longer time durations



(a)



(b)



(c)

Figure 4.5: Cross-sectional SEM images showing the development of oxide layer on 316 stainless steel as a function of exposure time in RG SC-CO<sub>2</sub> at 650°C, (a) 200 hours, (b) 600 hours, and (c) 1000 hours.

# Corrosion Resistant Overlay

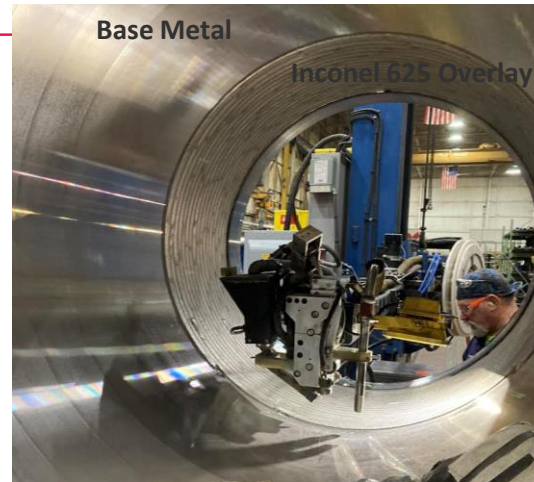
- Option for minimizing costs of compressors casing or storage tanks is to apply a corrosion resistant alloy on carbon steel (cladding)





# Inconel 625 Overlay for Compressor Casings

- Utilized for highly corrosive environment
- Outer casing overlaid with Inconel 625
  - 8 mm thick overlay
  - Includes all surfaces contacting process gas
- Impellers are machined through 1-piece construction



Inconel 625 Overlay Being Applied to Compressor Barrel Forging



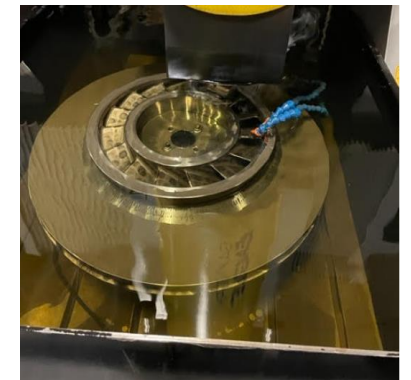
Overlay of Compressor Nozzle



Casing with Overlay Ready for Stress Relief



Endwall Overlay



EDM Machining of 1-Piece Impeller

# Low Temperature Considerations for Centrifugal Compressor Casings

- Centrifugal compressor casing material selection is heavily influenced by the Minimum Design Metal Temperature (MDMT)
  - Liquefied CO<sub>2</sub> can be below room temperature
  - API 617 – 8<sup>th</sup> Edition Annex D provides typical materials
    - Based upon ASME BVPC Section VIII
- Purpose it to ensure that casing materials will remain ductile at the lowest possible temperatures the casings will be exposed to



Multi-Stage Centrifugal Compressor Casing

# Slip Planes Provide Ductility

- Slip planes allow layers of atoms to slide past each other
  - These planes are thermally activated in Body-Centered Cubic Structure
  - Slip planes are always active in Face-Centered Cubic Structure

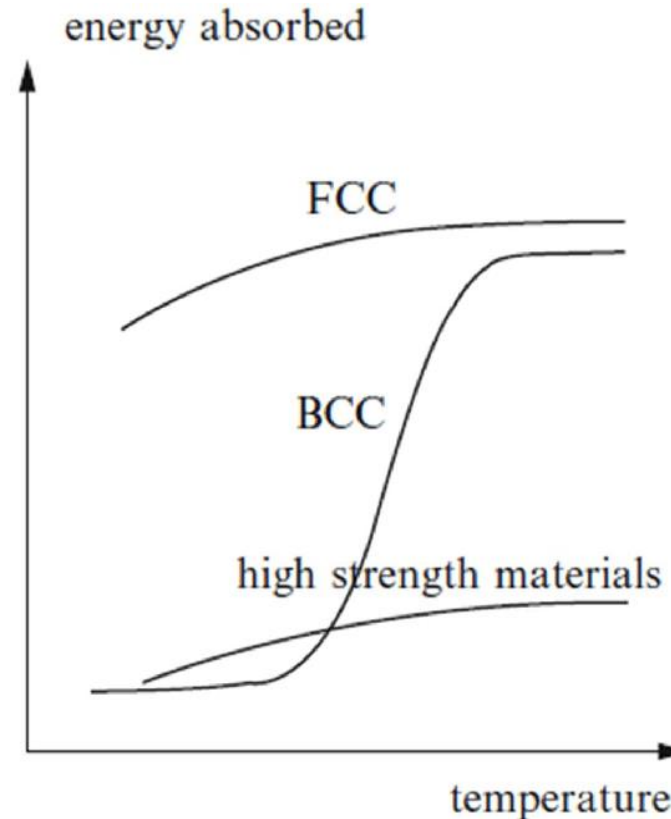
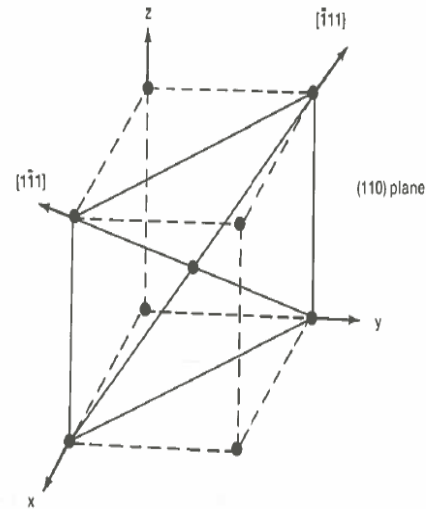
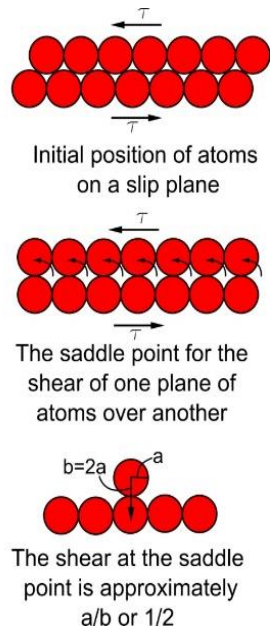
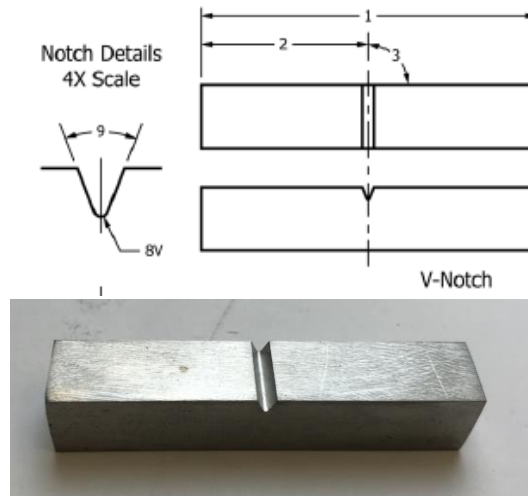


Illustration of Slip Planes  
within a Metallic Material



# Testing the Toughness of Steel and Other Alloys

- Charpy V-Notch Impact Testing



Standard Charpy V-Notch  
Impact Specimen

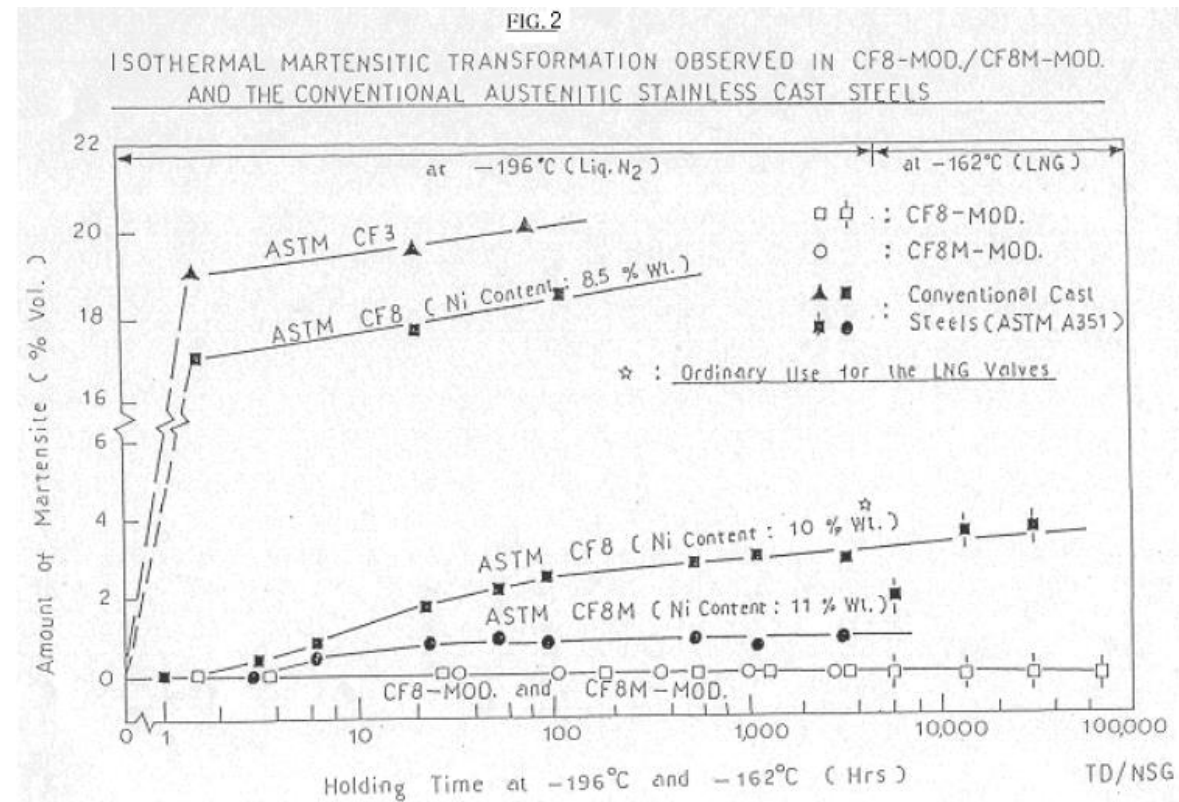


Charpy V-Notch  
Impact Specimen  
submerged in cooling  
bath at required  
testing temperature



Charpy Impact  
Tester

- Austenitic stainless steel castings require additional consideration for low temperature applications



# Thank You !